

# พันธมิตรนวัตกรรม เพื่อธุรกิจพลังงานไทย

## Technology Partners

BakerHughes



## Market & Trusted Customers

- E & P
- PETROCHEMICAL
- REFINERY
- GAS



More Information

Please Contact :

Tel : +66 2 260 1295

Email : [inquiry@bepetrothai.com](mailto:inquiry@bepetrothai.com)



# Engineering Management Service

## Customer

- Requirement/ Problem
- Information
- Plant/ process data
- Operating data

## Manufacturer

- Technology

## Feasibility Study

### Fact Finding

- Customer requirement/ Pain point
- Process flow
- Equipment function

### Assessment

- Information survey
- Site survey

### Find out Solution

- Simulation
- Technology selection

## Conceptual Design

- Technology
  - Technology selection
  - Benefit
- Constructability
  - Construction works
  - Limitation & Modification work required
- Budget +/-30%

## Customer

- Product specification
- Engineering Standard

## Manufacturer

- Product Sizing & Selection
- Engineering Standard

## Detailed Design

### Engineering Design

- Sizing and selection

### Engineering Alignment

- Engineering standard & Project specification
  - Design & Specification
  - Source of material
  - Production & Testing

## Scope of Supply

- Scope of Supply
  - Goods : itemized
  - Service : activities
- Detailed Engineering
  - Preliminary datasheet and drawing
  - Bill or quantity
  - Vendor document schedule
- Project schedule
- Budget +/-10%

## Manufacturer

- Procurement :
  - Sub - vendor
- Production

## Contractor

- Service
  - Inspection
  - Construction service
  - Commissioning & Performance test
- Resource
  - Manpower
  - Tools

## Project Execution

### Engineering

- Quality engineering
- Safety engineering

### Resource Management

### Execution

- Goods : Production & Testing
- Service : Installation & Commissioning

### Progressive Measurement

### Risk Management

## Successful Contract

- Quality control
- Safety control
- Time control
- Budget control

### ITP & Work Procedure

### Resource Plan

### Progressive Report

### Recovery Plan



## Energy Recovery

Reuse Waste Heat to Power

- Organic Rankine Cycle
- Waste Heat Recovery



## Energy Saving

Reduce GHG

- XP Flare
- Column Internal Improvement
- Twisted Tube
- Radiant Coil SCOPE HT E



## Carbon Capture Utilization & Storage

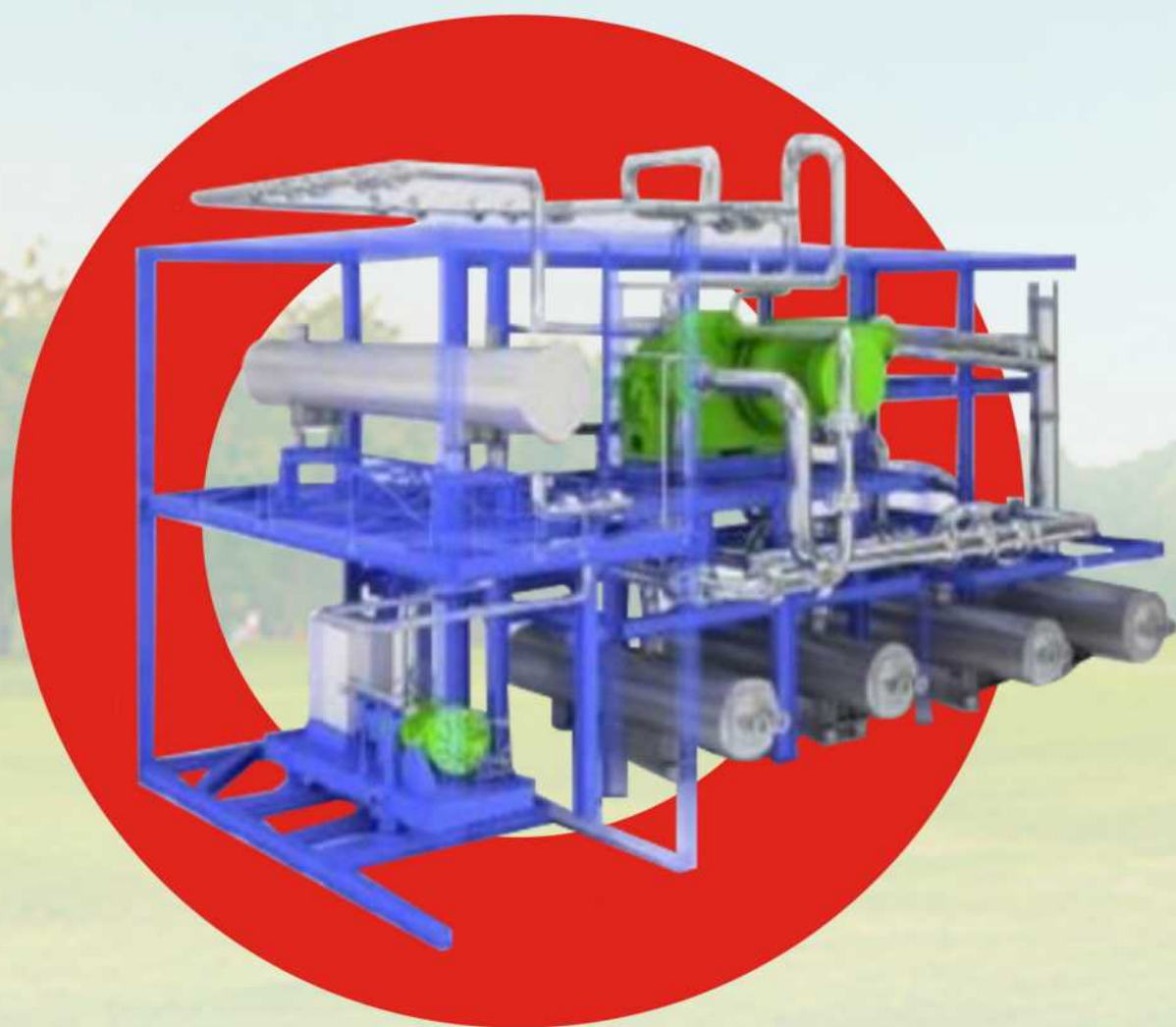
Reduce CO<sub>2</sub>

**System**

- NET Power Technology

**Machinery**

- CO<sub>2</sub> Gas Compressor
- CO<sub>2</sub> Liquid Pump



## New Energy

Replace Hydrocarbon to H<sub>2</sub>

**Power Generation**

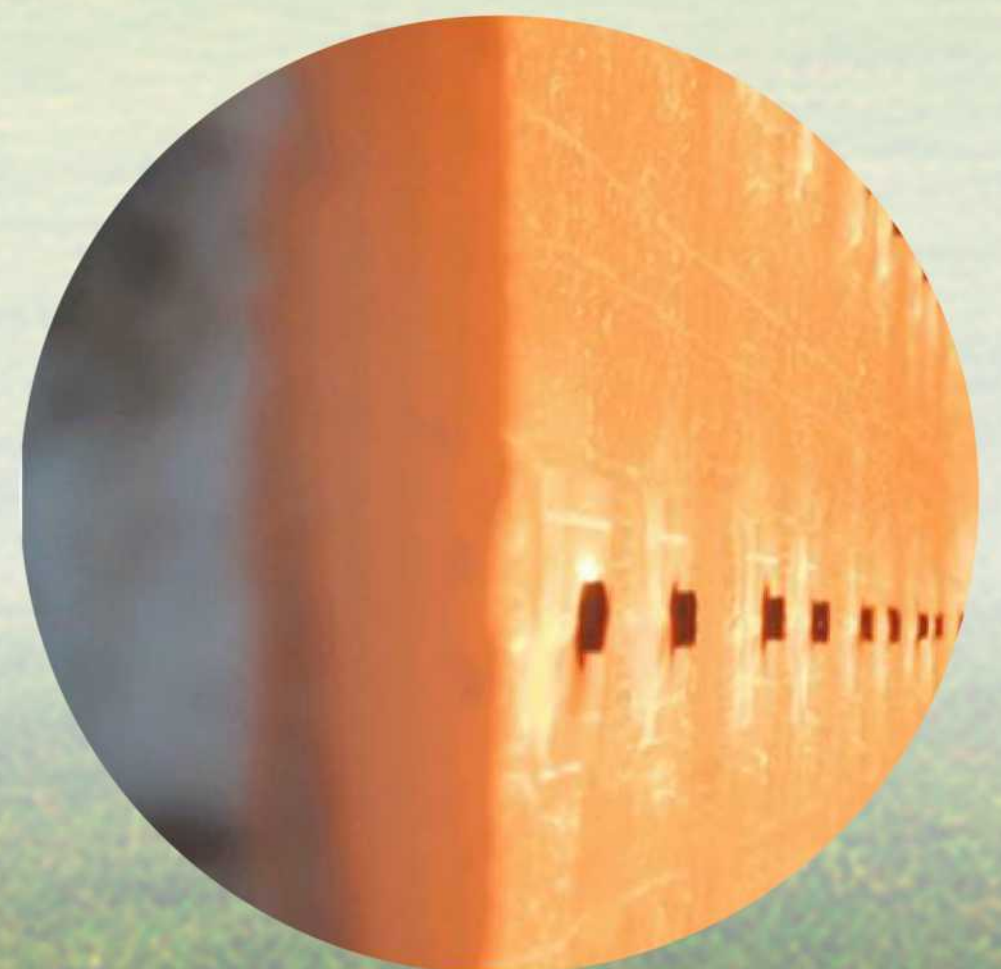
- Hydrogen Gas Turbine

**Combustion Process**

- Hydrogen Burner

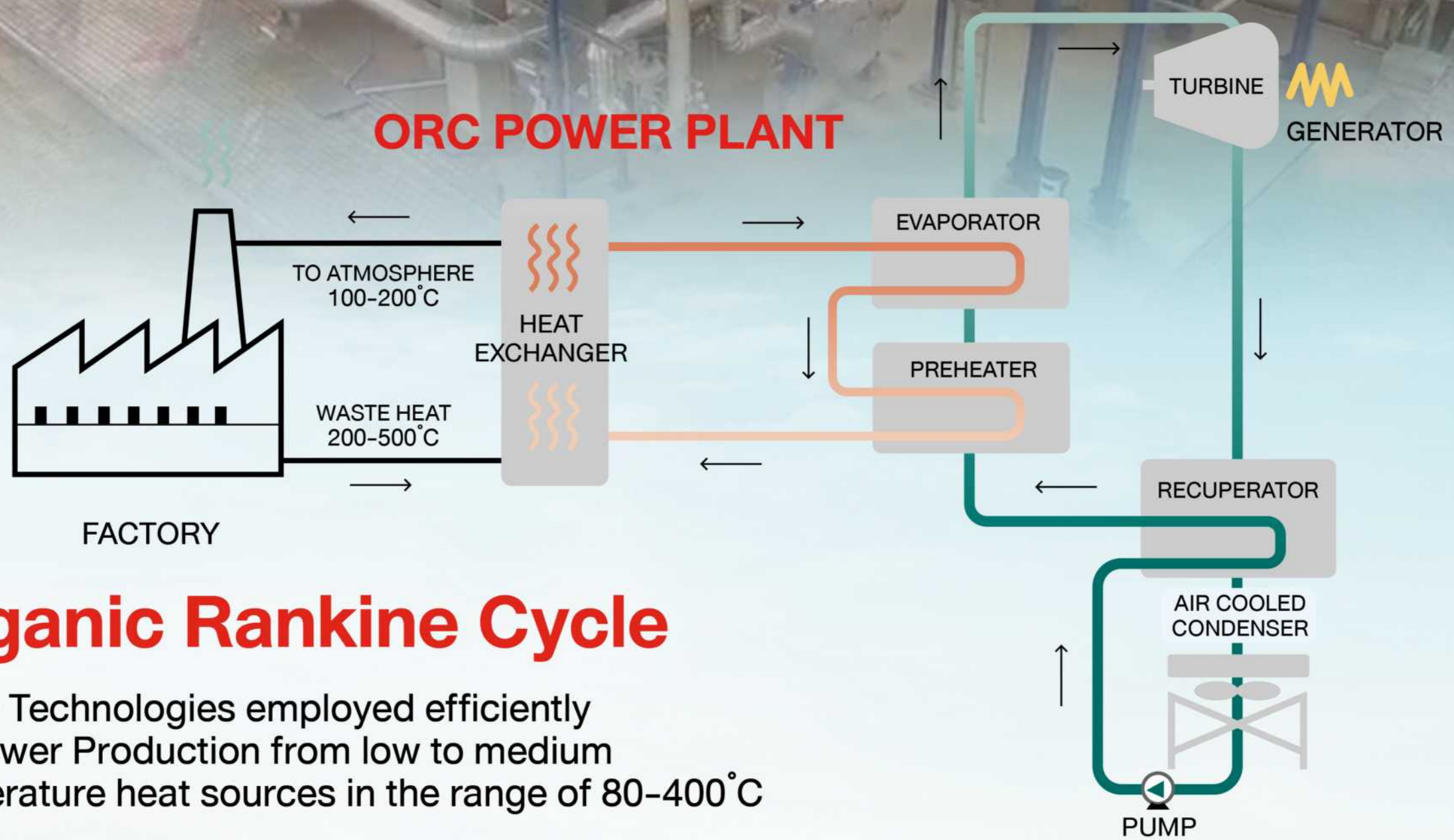
**Production Plant**

- Hydrogen Generator





# Organic Rankine Cycle



## Organic Rankine Cycle

(ORC) Technologies employed efficiently for Power Production from low to medium temperature heat sources in the range of 80-400°C

## Waste Heat from Industry

- Geothermal
- Flue Gas from Incinerator/Thermal Oxidizer
- Steel Plant
- The plant with waste heat
- Cement
- Sugar Mill

## Advantages

- No need of operators thus lower running cost
- No limitations and constraints on placement, better fitting available soil and production process requirements
- Higher amount of productive hours
- Easy maintenance
- No need of water consumption
- High Sustainability
- Possibility to exploit the maximum energy available from the process
- Low maintenance
- Higher Efficiency of the turbine
- Optimal match with the release curve and better operation at partial loads
- Lower power specific cost
- Lower operation and maintenance costs

## Case study

- Plant size : 5MWe
- Application : Heat Recovery Gas Turbines
- Heat Source Temperature (Diathermic Oil) : 294°C - 140.8°C
- Water or Cooling Agent : Cold water from LNG regasification cycle as heat sink
- Temperature Water : 5-38°C
- Environmental Savings : <23,460tCO<sub>2</sub>/y
- : <7,497 TOE/y





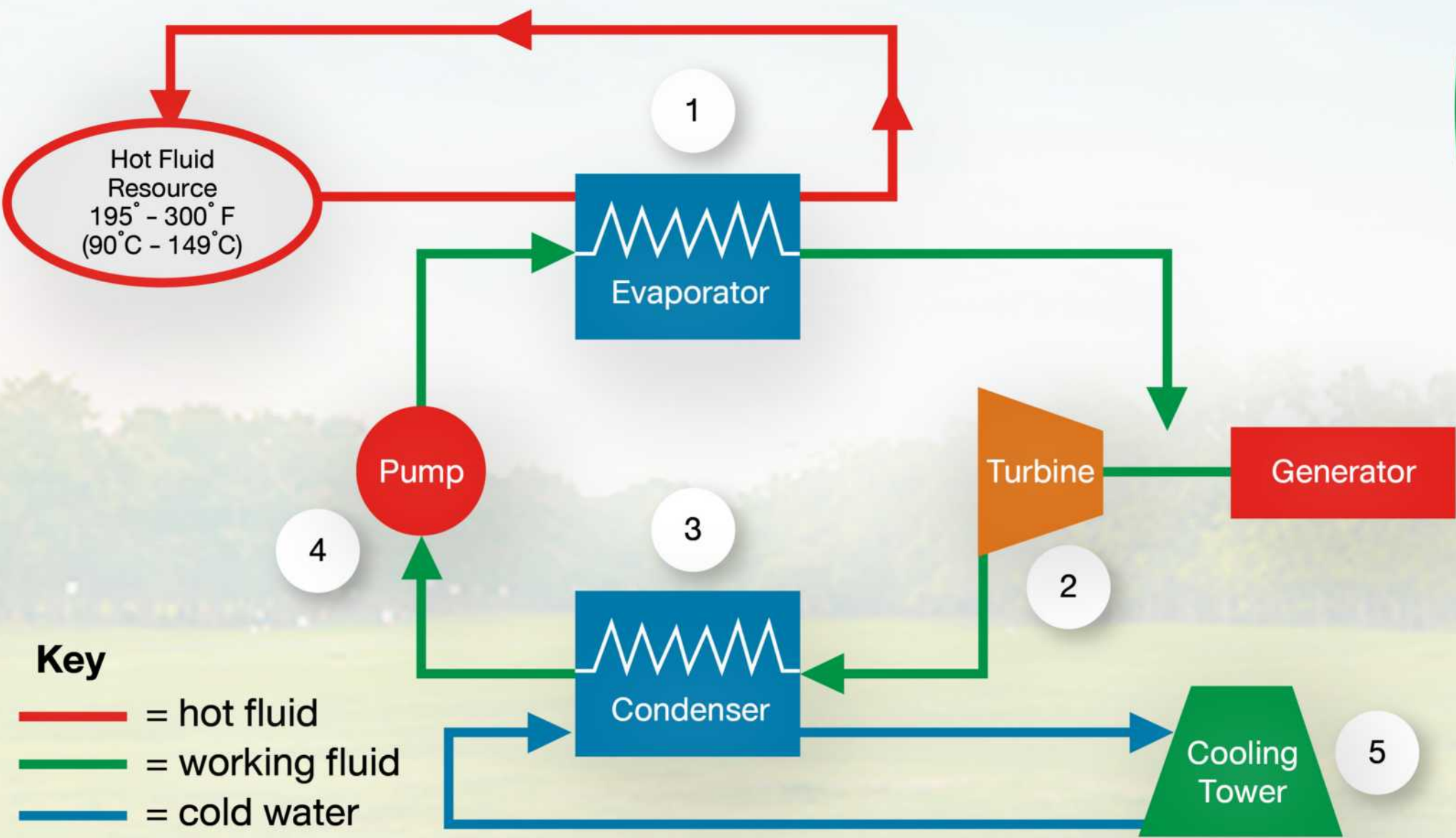
Organic Rankine Cycle  
**Pure Cycle**  
Standard Package

**Specification**

Size :	5.8 x 2.3 x 3.5 m
Output Power :	272/280 kW
Frequency :	50/60Hz (Customer determine)
Voltage :	380 ~ 460V (Customer determine)
Heat Source :	Steam
Heat Temperature :	101~150°C
Heat Flowrate :	2.5 ~ 5 t/h
CW inlet temperature :	25 ~ 35°C (Change with the ambient)
CW Flowrate:	300t/h (Delt T = 8°C, for each unit)
Empty Weight :	14 t / unit
Operating Weight :	17 t /unit



**System Operation**



In the Specified conditions, the expected performancesof **TICA’s ORC Purecycle 280 units** are following :

	Hot Source				Cooling Water		Power Output		
	Inlet Temp. °C	Inlet Press. KPa.a	Outlet Temp. °C	Flow Rate t/h	Inlet Temp. °C	Outlet Temp. °C	Flow Rate t/h	Gross kW	Net kW
Unit 1	126	500	80.6	55	30	35	465	245.2	228
Unit 2	126	500	80.6	55	30	35	465	245.2	228
Unit 3	126	500	80.6	55	30	35	465	245.2	228
Total				165			1,395	735.6	684



# Waste Heat Recovery Unit

A reputation for engineering excellence, quality and responsiveness to individual client's expectations.



Case study : Distribution Plant

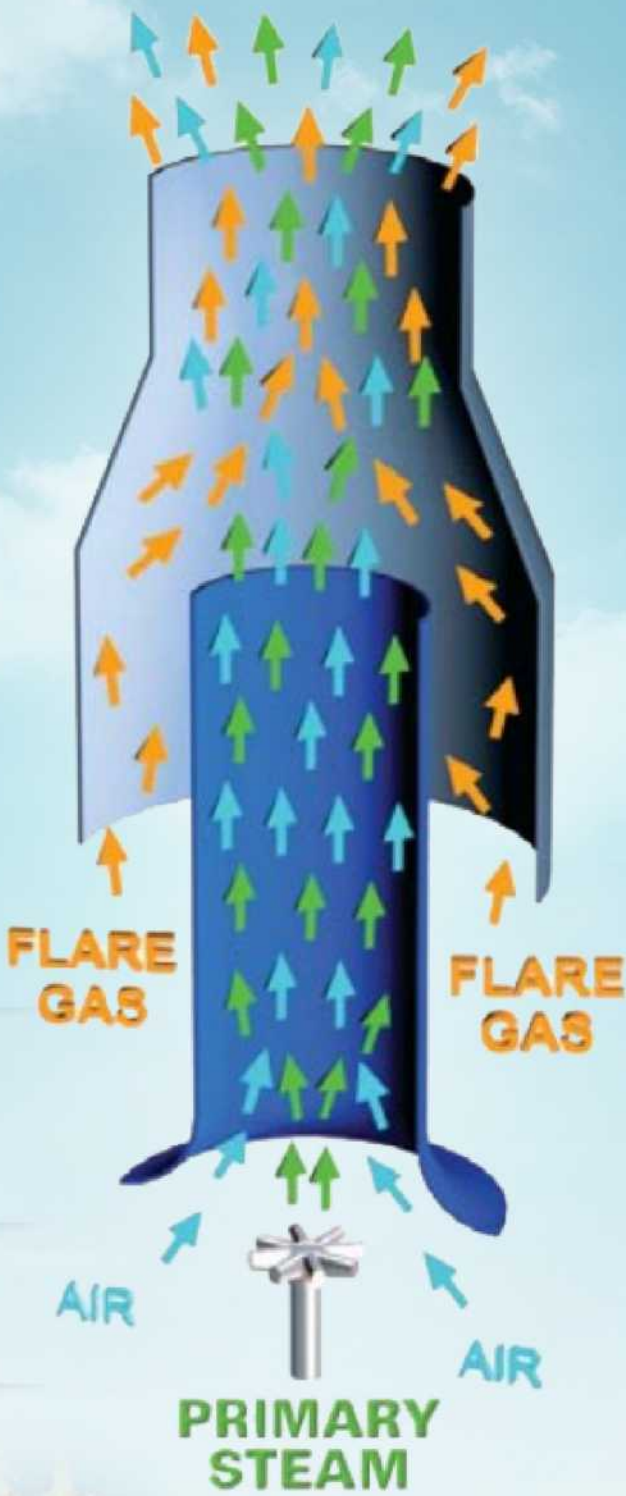


XP Flare

Steamizer XP

- Minimize Smoke
- Reduce steam consumption
- 30% - 40% less steam for smoke suppression

40% - 60%  
Increased smokeless  
capacity for a given  
steam flow rate



FEATURES

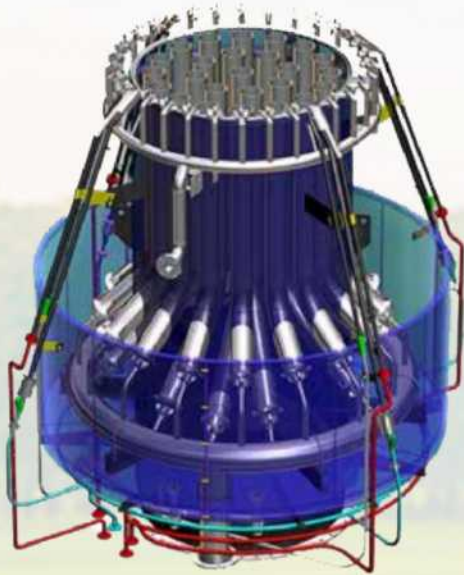
- Ultra-high smokeless capacity
- Low noise design
- Eliminates steam capping
- Low steam/gas ratio for smokeless flaring
- Single steam-line option
- No center steam required
- Ultra-low minimum steam capability

BENEFITS

- Minimizes environmental / community impact of flaring
- Extended tip life
- Reduced steam consumption
- Simple operation
- Minimizes over-steaming
- Significantly reduced steam capability



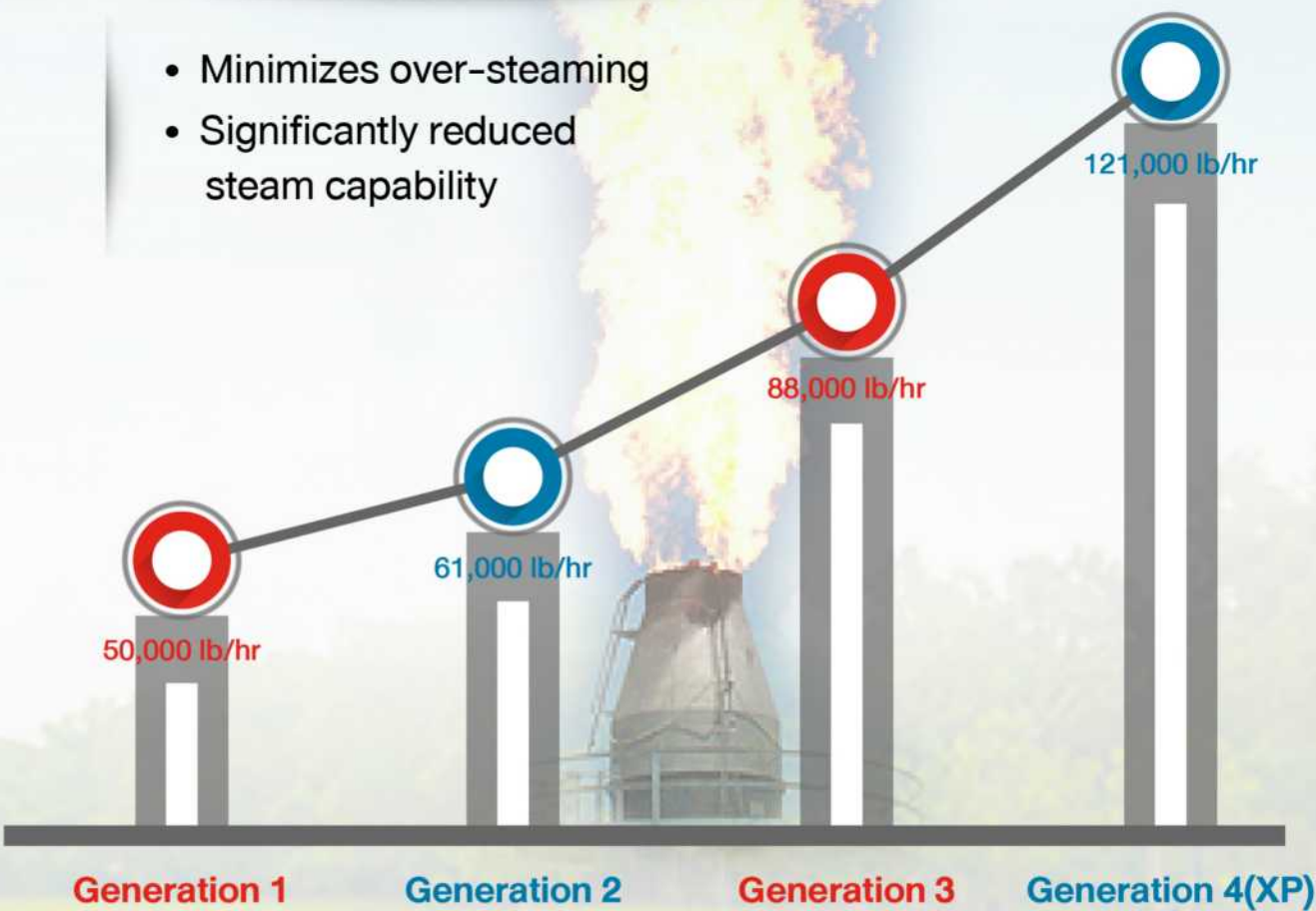
Traditional



Steamizer HSA  
Flare tip

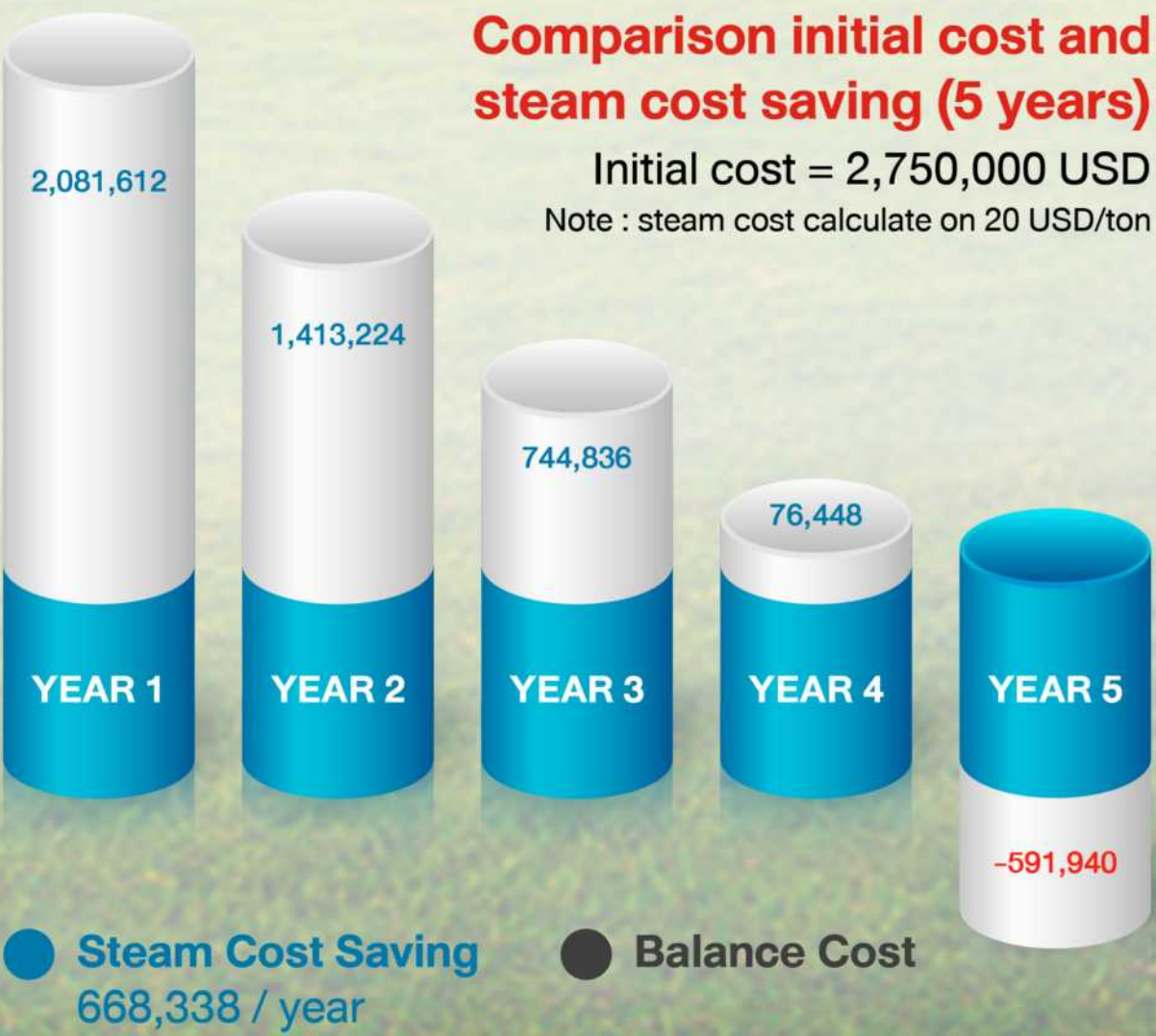


QS  
Upper Steam Flare



Propylene Smokeless Performance  
Flow Rate (lb/hr)

Case Study : Aromatic Plant  
Equipment : XP Flare



Comparison initial cost and  
steam cost saving (5 years)  
Initial cost = 2,750,000 USD  
Note : steam cost calculate on 20 USD/ton

Steam Saving	Existing Flare Tip	XP Flare tip with Reduced steam (CSR)
Smokeless R0 % of max capacity	8% (135tph)	10% (168tph)
Smokeless R1 % of max capacity	10% (170tph)	13% (221tph)
Cooling Steam	3,200 kg/h	500 kg/h
Purge Gas	18.6 M3/h	74.5 M3/h
Yearly Steam Saving	-	33,419.4 tons
6years CO <sub>2</sub> saving (vs existing technology) TCO <sub>2</sub> e		32,000 tons (approx.70% Reduction)



TWISTED TUBE®  
Bundle Construction

- Tubes are firmly supported.
- Vibration Free : Vcr > 305 m/s (1000ft./sec)
- No single tube can vibrate.

= Overall Heat Transfer Rate

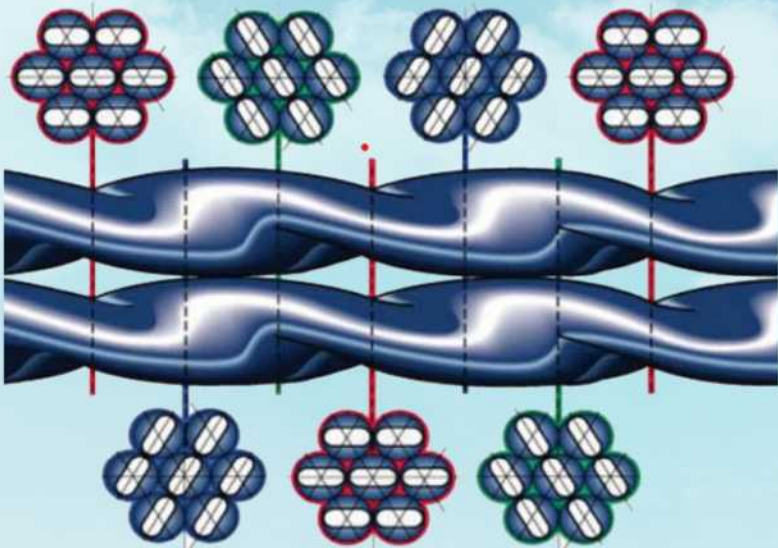
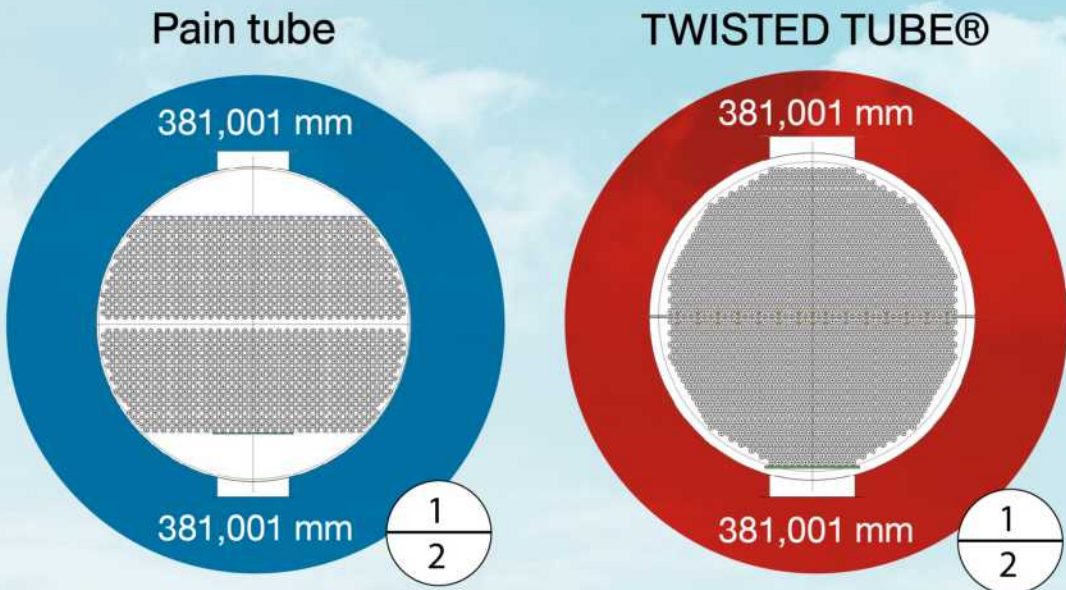
= Heat duty

$$Q = U_0 * A * F * LMTD$$

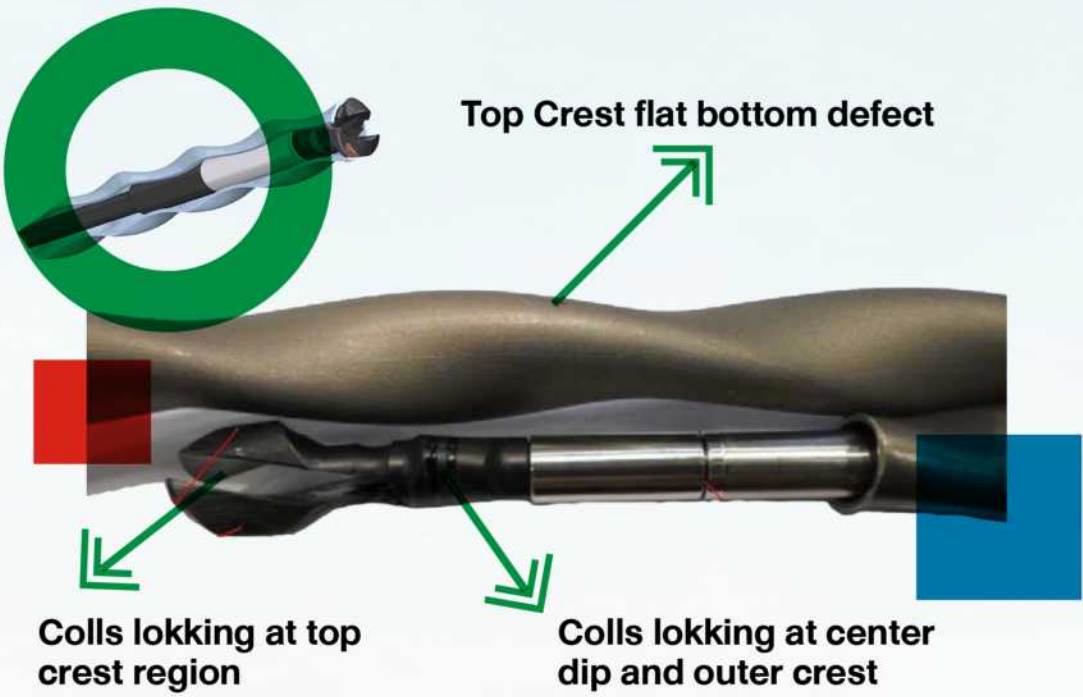
= Temperature Correction Factor

= Log Mean Temperature Difference

= Surface Area



Inspection



TECHNICAL INFORMATIONS

INSPECTION EQUIPMENT			
BRAND:	Eddyfi	SOFTWARE:	Magnifi
MODEL:	Ectance 2	TECHNIQUE:	RFT (Twistec probe)
PROBE:	6 mm.	FREQUENCY:	2.8 KHz.

CLIENT/EQUIPMENT DETAILS			
CLIENT:	PTT GSP	LOCATION:	GSP6 plant
EQUIPMENT NO:	3603-E003A	MATERIAL:	A-179
TUBE SIZE (ODxWT):	19.05 x 2.11 mm.	TOTAL TUBE:	4750
LENGTH:	6000 mm.	INSPECTED TUBE:	395
TEST SIDE:	Tube sheet / Front	TEST DATE:	11-12 JULY 2021

Cleaning



SHELLSIDE PRE-CLEANING

- Remove shroud
- Do not remove bands

SHELLSIDE HYDROBLASTING

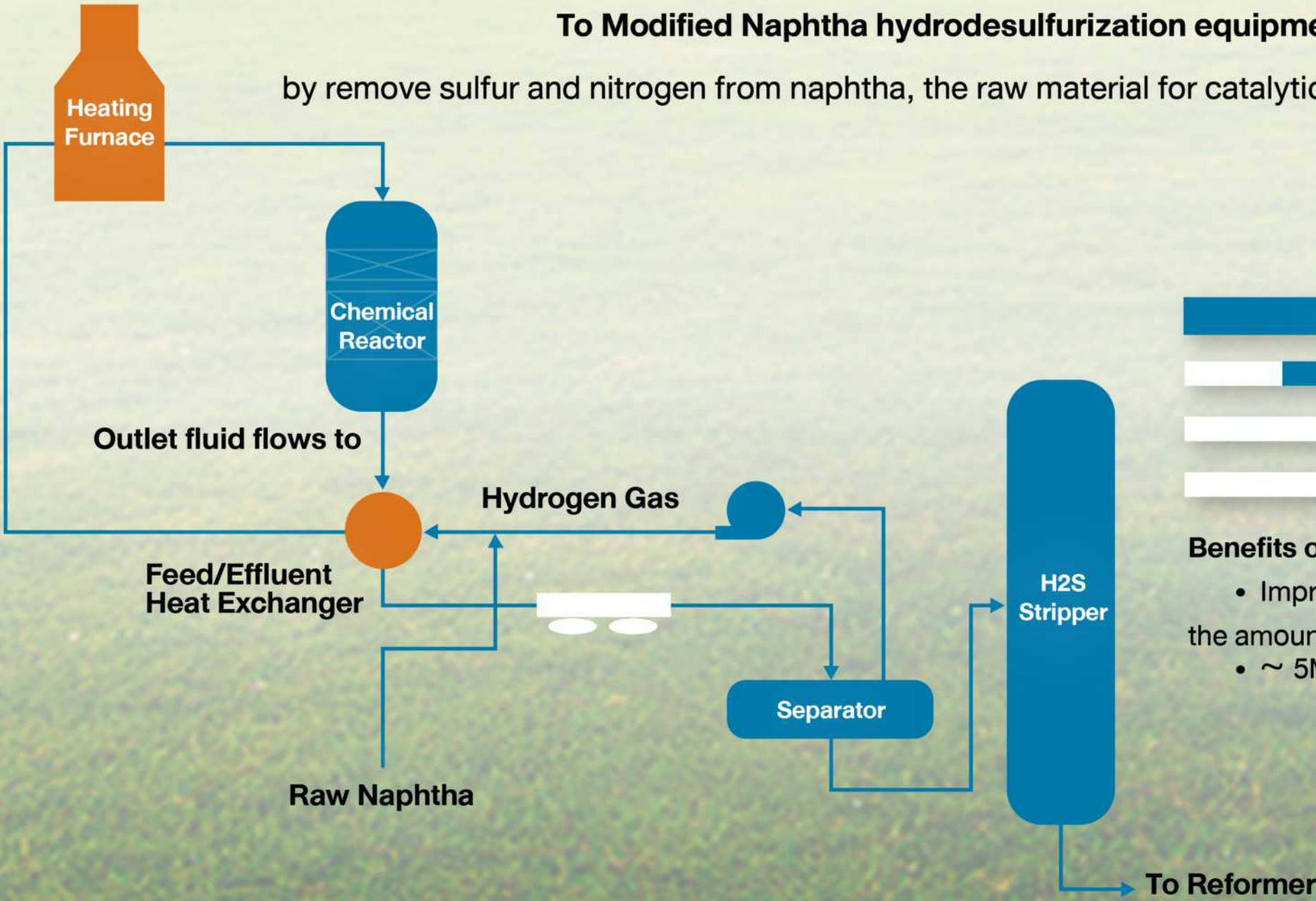
- Cleanable triangular pitch bundle due to cleaning lanes.



Case Study : Refinery Plant

To Modified Naphtha hydrodesulfurization equipment

by remove sulfur and nitrogen from naphtha, the raw material for catalytic reforming equipment



Before		After	
1,914	Heat Transfer Area (M2)	3,586	
350	Overall Heat Transfer Coefficient (W/m2 K)	395	
10	Heating Furnace Combustion (MW)	5	

Benefits of modification : Energy Conservation

- Improved heat transfer efficiency reduces the amount of combustion in the heating furnace
- ~ 5MW Energy savings



# Column Internal Improvement

- Decrease Reboiler / Condenser Energy
  - Decrease Fuel Cost
  - Decrease Steam Consumption
- Increase Turndown Ratio
- Increase Capacity / Efficiency



**FLEXITRAY®**  
Valve Trays



**FLEXIPRO®**  
Valve Trays

## Next Generation FLEXIPRO® valve trays

- Capacity increase up to 30%
- Enhanced push and sweeping effect over the tray deck to remove solid deposits - Mitigates the risk of fouling and achieves longer run lengths
- Fixed valve - Increased reliability
- Fixed valve - Uniform vapor distribution maintains tray efficiency over the full operating range

## INTALOX® ULTRA Random Packing

Bridging the gap between capacity and efficiency.

An innovatively designed structure that maximizes the effective surface area.

The low pressure drop and high capacity of this packing:

- Allows smaller diameter for new columns
- Reduces energy consumption
- Reduces foam generation
- Reduces pressure drop
- Increases capacity



## SUPERFRAC® High Performance Trays

The SUPERFRAC® tray is a high performance cross-flow tray that has the highest combined capacity and efficiency of all single-pass cross-flow trays tested at Fractionation Research Inc. (FRI)

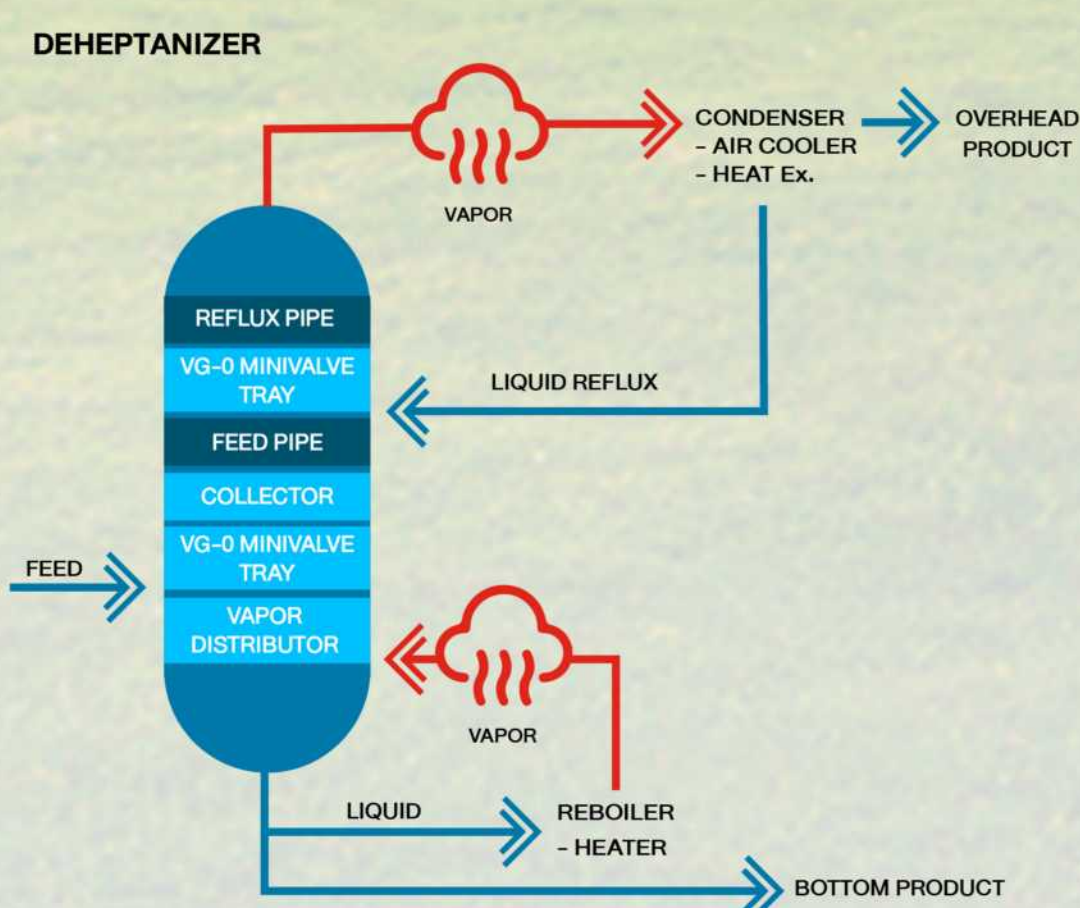
- Advanced downcomer technology
  - Active area enhancements
  - Inlet area enhancements
- Increase capacity and efficiency

### Case study#1

Column : Deheptanizer  
7 % Increased capacity  
12.60% saving

### Case study#2

Quench Oil Tower  
Plant : Olefin



Random packing :  
Cascade miniring



Random packing :  
Intalox Ultra

New generation high performance packing facilitates  
13% additional capacity  
36% reduction in overall pressure drop



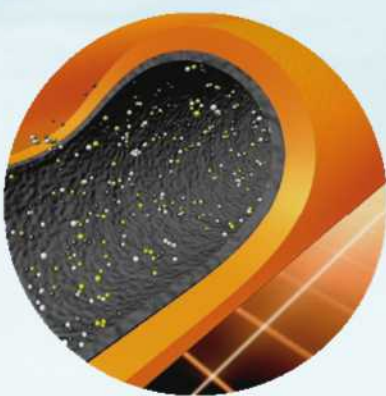
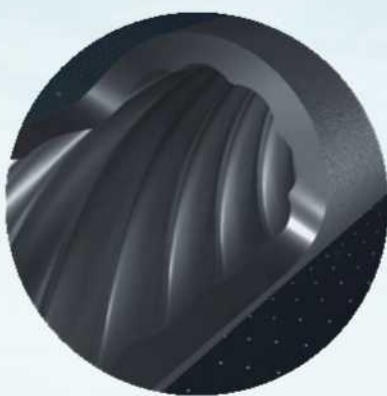
# Radiant Coil SCOPE HT E

Longer Runs – Lower Coking Rates

Longer Runs  
Lower Coking Rates



BARE TUBE

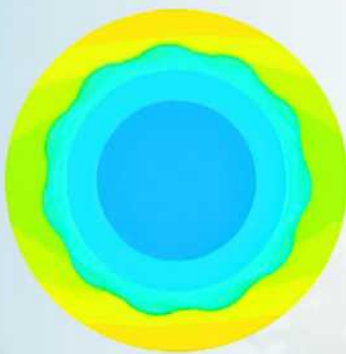
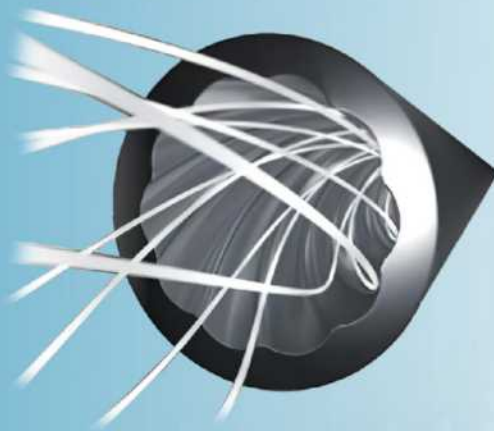


Rotating Flow Pattern

- Improved heat distribution across tube shell
- Reduced gas temperature gradients
- Balancing of sunny/shady sides
- Less carburization/maintenance
- Customizable profile (amount of fins & profile depth)

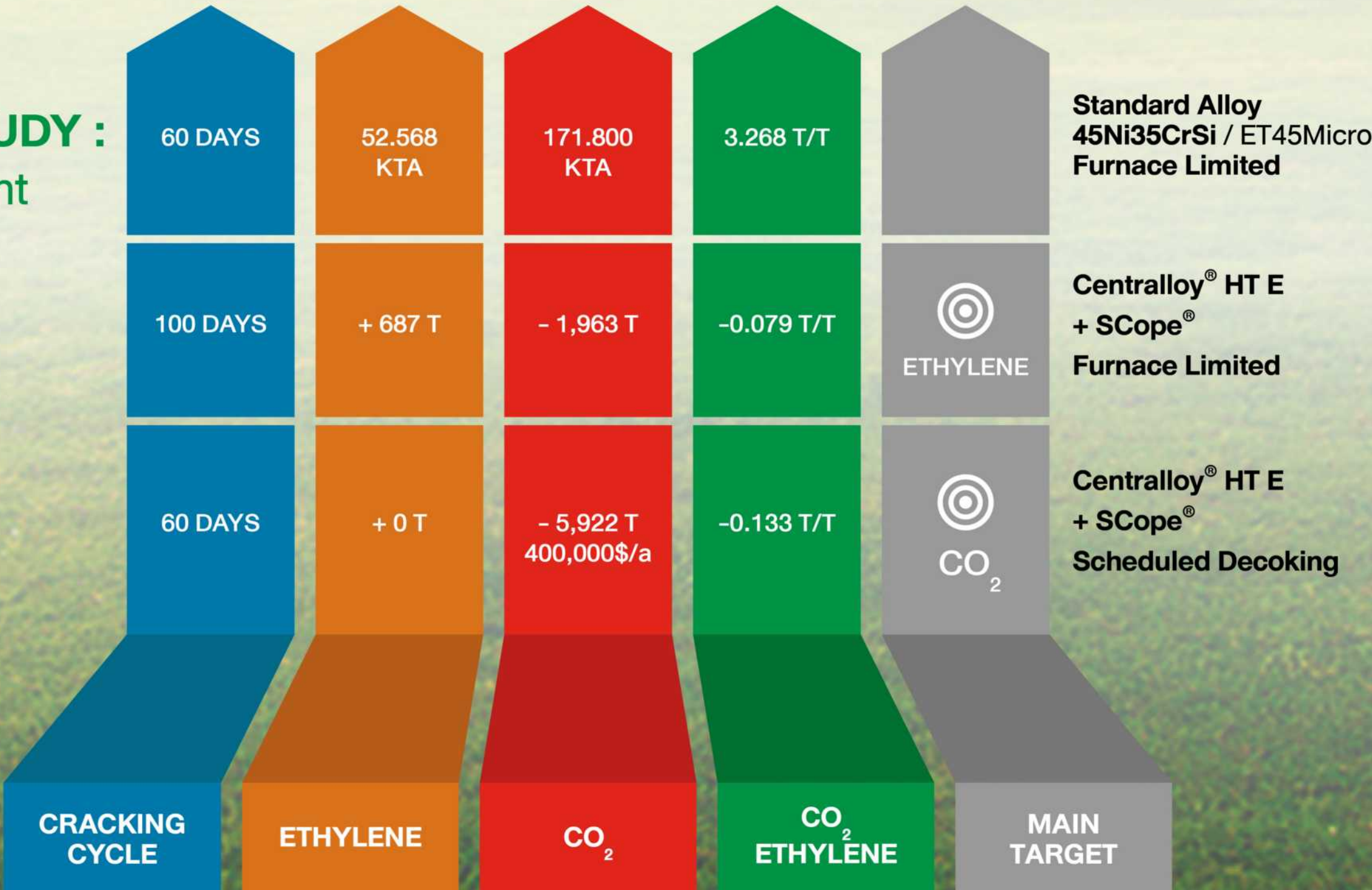
## Performance

- **Increased run length** (lower TMT & coke formation) by factor of ~1.5 to 2
- **Higher product selectivity** (gas temperature balancing, less over-/undercracking) ~1% more olefins
- **Increased energy efficiency or higher feed rate/conversion potential** (higher heat transfer) ~3% fuel saving or ~+10% feed rate or ~+2% conversion (base on identical cooking rates)
- **Increase coil life** (Lower tube temperatures, less carburization)



## Efficiency Improvement Standard Material vs HT E + SCOPE

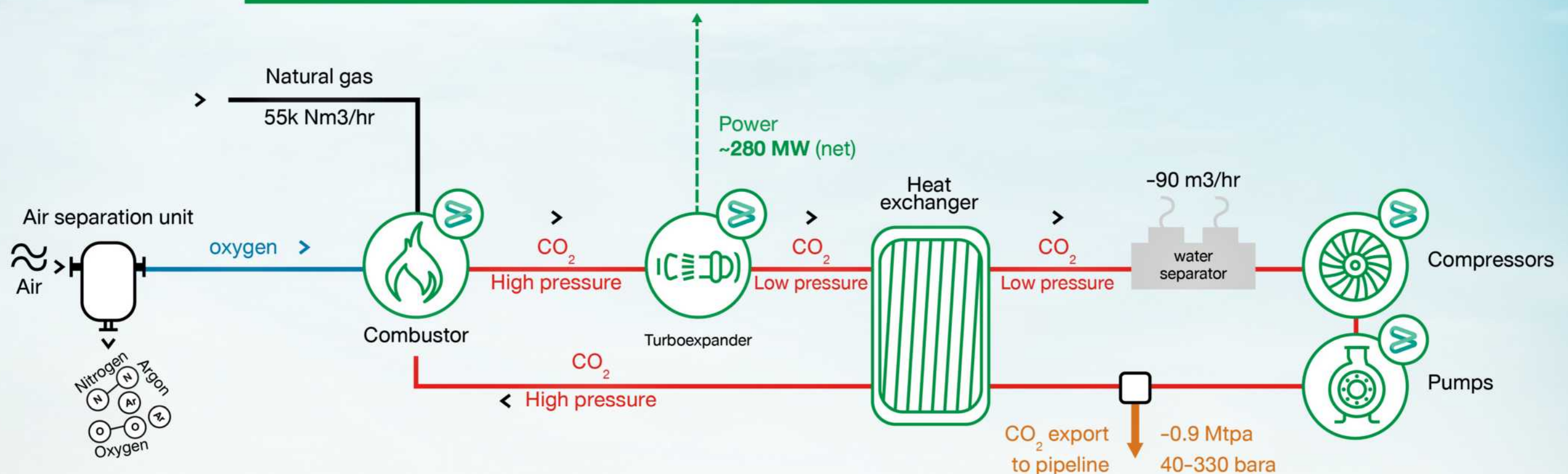
### CASE STUDY : Olefin Plant





# System NET Power Technology

## How its Work



- Traditional plants burn nature gas in air, producing diluted CO<sub>2</sub> and NO<sub>x</sub>, which make CO<sub>2</sub> separation expensive and efficiency-robbing.
- NET Power plants use **oxy-fuel combustion**, combusting pure O<sub>2</sub> with methane, and continuously recycle a stream of CO<sub>2</sub> in a loop.
- By eliminating the N<sub>2</sub> NET Power platform makes **CO<sub>2</sub> separation as easy as simply spilling it** already at high pressure and high purity, ready for transportation and storage.
- In addition, an intimate heat integration network reduces waste and increases all-in ISO **efficiency above 50%.**



Machinery  
CO<sub>2</sub> Liquid Pump

Super Critical CO<sub>2</sub> Characteristics and Pump Selection



CO<sub>2</sub> Compressibility  
Low Viscosity

**Rotordynamic**  
low damping effect

**New Impeller Family**  
density variation up to 25%

**Acoustic Resonance**  
different fluid characteristics

**Performance Assessment**  
validation for liquid and critical CO<sub>2</sub>

Benefits

Speed and rotor stability

Maximized Pump Delta P

Wet and Dry seals available

Water vs CO<sub>2</sub> correlation laws

Customer Value

Efficiency and footprint

Optimized seal technology selection

Accuracy of the performance prediction



## Machinery

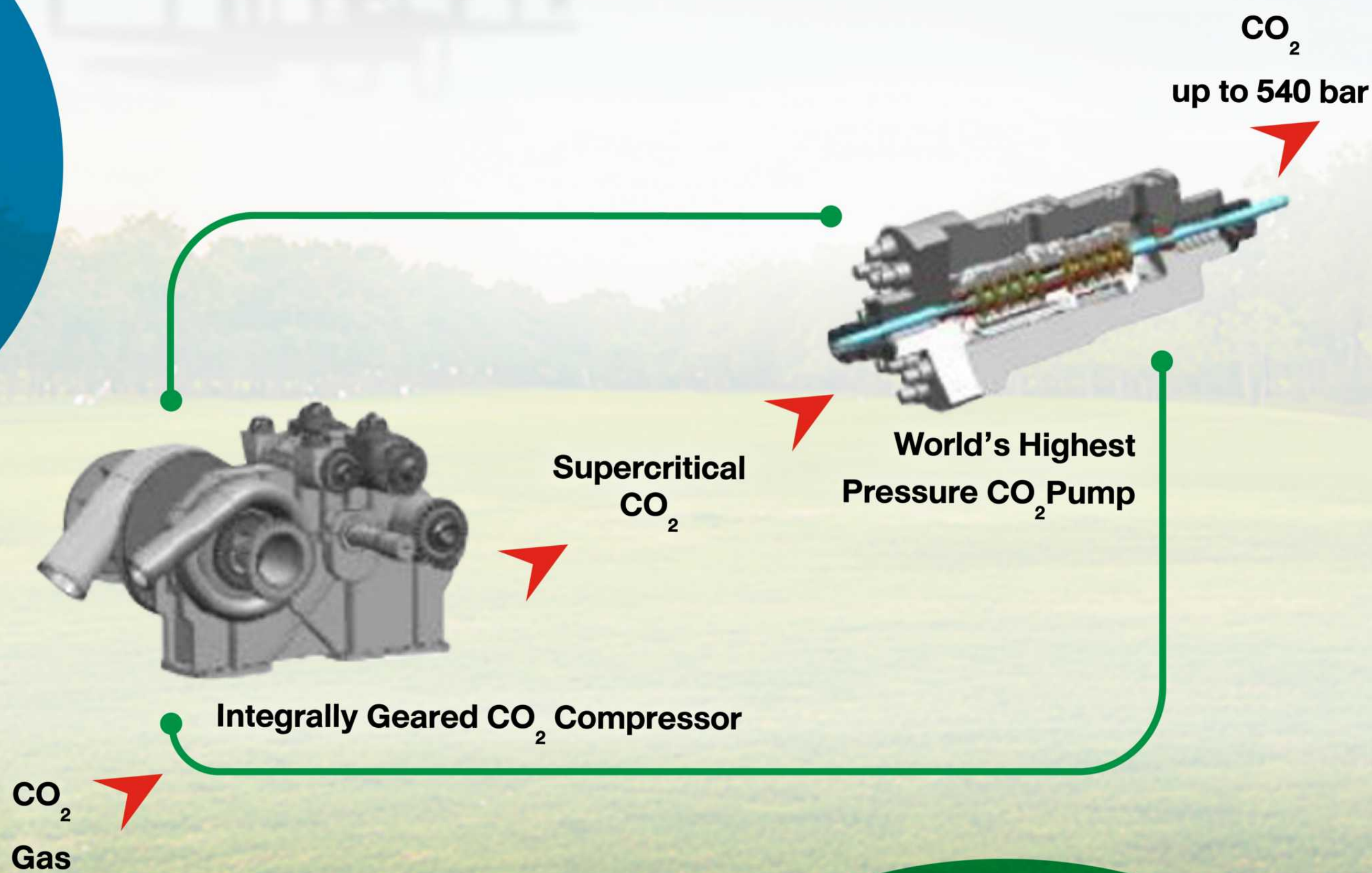
# CO<sub>2</sub> Gas Compressor

Modular integration CO<sub>2</sub> system for easier installation & operation



### UNIQUE BH CAPABILITY Advantages & Compressor only

- 10% Less Power
- Operational Flexibility
- Common Controls & Auxiliaries
- Reduced CAPEX/OPEX
- Smaller Footprint

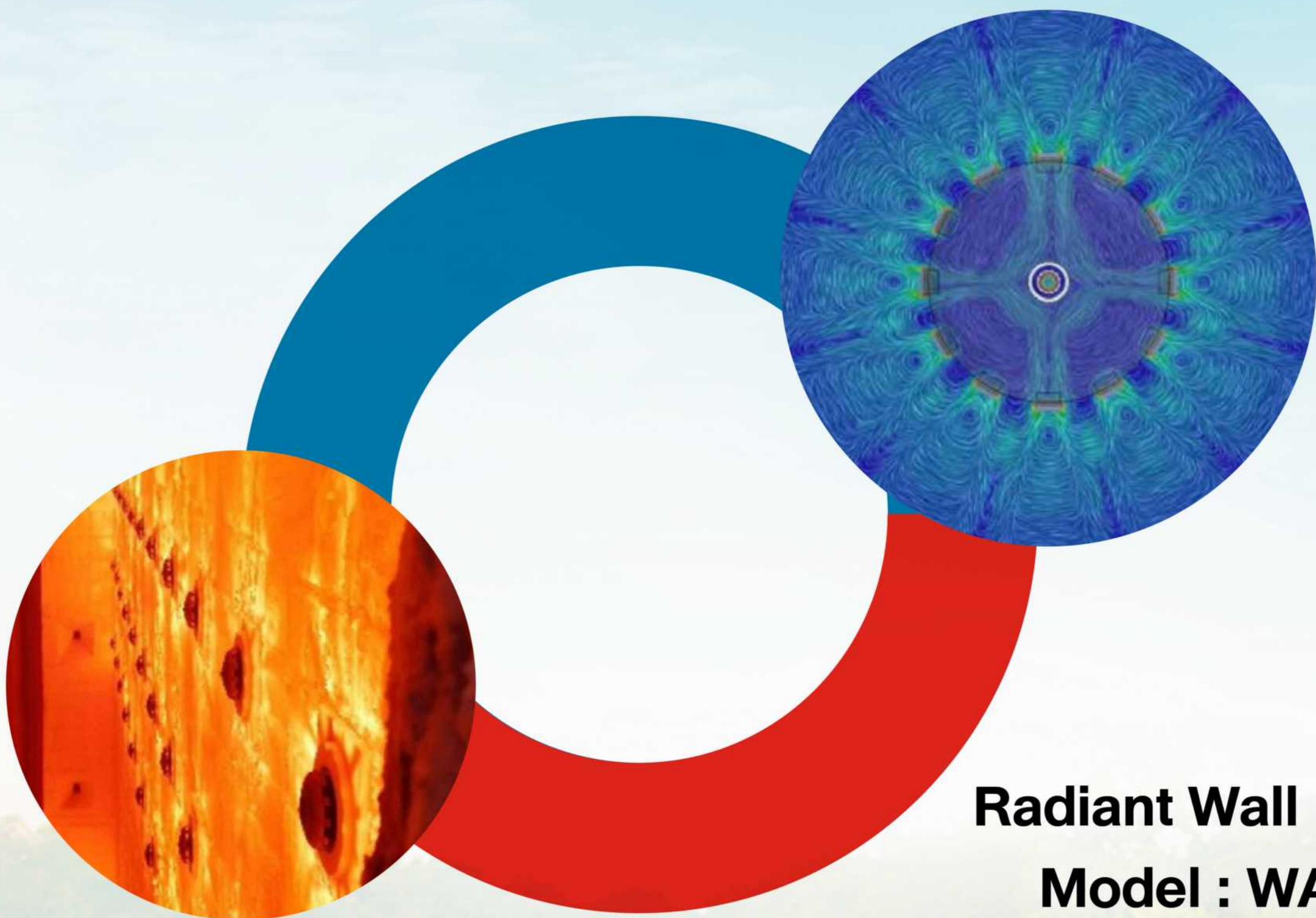




# Hydrogen Burner

The WALFIRE burner draws upon decades of radiant wall burner experience in reforming and olefins furnaces across the globe to deliver superior performance and benefits.

- +100% No-flashback guarantee, due to diffusion concept
- +The lowest possible NOx emission for such applications



**Radiant Wall Burner  
Model : WALFIRE**

## Performance

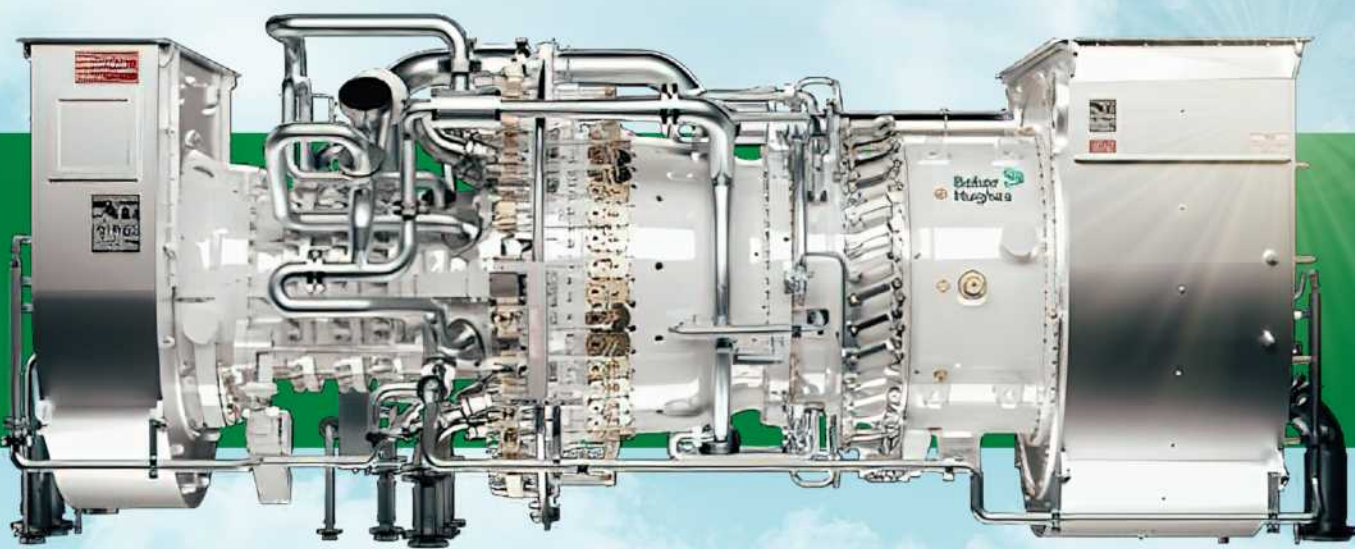
- Less than 82 dBA noise at 3ft or 1m
- Fuel flexibility including up to 100% hydrogen
- Extremely low gas pressure required <0.5 bar(g) for 0.3MW
- Specifically designed to provide a radial flame that lies flat against the fired wall preventing flame projection into the process coils
- Customizable flame geometry to fit tightest installations
- Very large air ports which are virtually impossible to plug during normal operating conditions (dust/sand)

**Case Study : 100% Hydrogen  
Duct Burner HRSG Plant**






# Hydrogen Gas Turbine

Model :  
**NovaLT™**



## Design to minimize total cost of ownership

- **Availability** > 99%
- **Best in class efficiency**, full and partial load
- **35,000 hours MTBM**
- **Maintainability** : engine swap in 24 hours
- **Remote Operability**

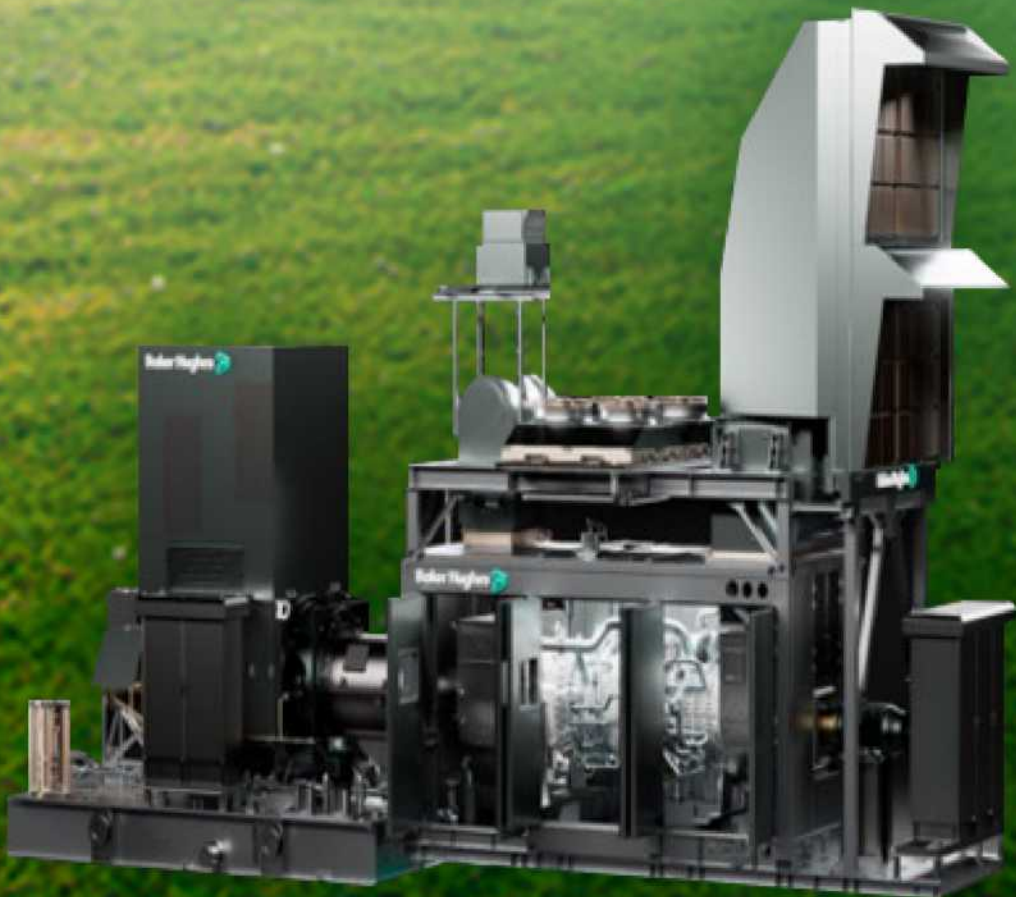
	 <b>LT5</b>	 <b>LT12</b>	 <b>LT16</b>
Shaft Output	5.5MWe	13MW/12.5MWe	17.5MW/16.9MWe
Efficiency @ full load	31.5/30.7%	36.8/35.3%	37.5/36.4%
Efficiency @ 70 % load (feat. VATN LT12/16)	28.3%	32%	33.1%
Shaft nominal speed	16,630 rpm	8,900 rpm	7,800 rpm
MTBM	24,000 fire hours	35,000 fire hours	35,000 fire hours
NOX emissions	15 ppm	15 ppm*	15 ppm*

\*9 ppm available on request

## Case Study : Commercialize in Canada

Equipment : Gas Turbine NovaLT™16

Commissioning : **December, 2024**  
Start up : **Blends up to 100% H2. switch from NG to gas blends up to 100H2 on the fly**



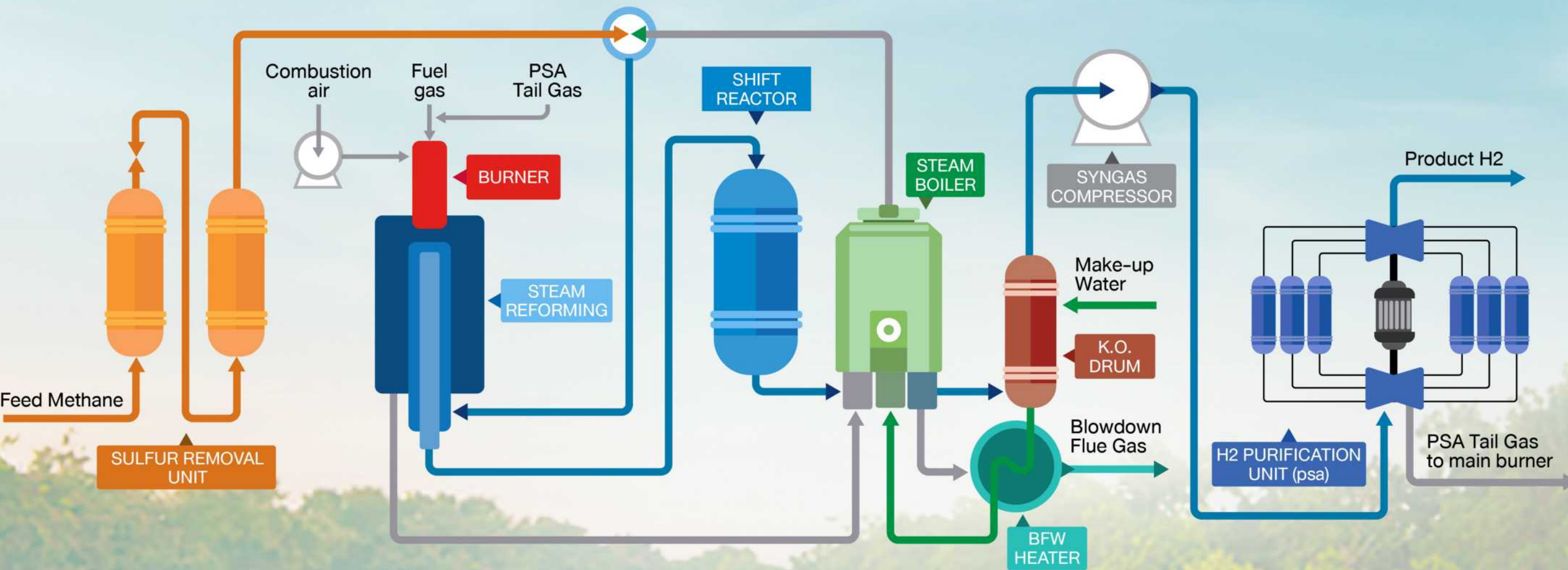
	Capacity	% efficiency
Powergen Simple Cycle	16.9 MWe	36.4% Elect. efficiency
MECH Drive Simple Cycle	17.5 MWe	37.5% Elect. efficiency
Combined Cycle	22.0 MWe	48% Elect. efficiency
Cogeneration (CHP)	31tph Steam output	80% CHP efficiency
Maintenance	35k-70k (FFH)	<ul style="list-style-type: none"><li>• No annual inspection</li><li>• Fast engine exchange</li><li>• Minimized inventory</li></ul>
Nox Emissions	<ul style="list-style-type: none"><li>• 15 ppm with SCR at exhaust (today)</li><li>• 15pp, DLN (From 2026)</li></ul>	



# Blue Hydrogen Generator



**Steam Methane Reforming (SMR) with Carbon Capture and Storage (CCS)** uses innovative and high efficient adsorbent media, producing Hydrogen from natural gas or biomethane while capturing resulting carbon dioxide emissions. Therefore, SMR with CCS is a promising technology for reducing greenhouse gas emissions from Hydrogen production.



## Input Feed & Fuel Specifications

Natural Gas Analysis Pressure : 1 bar(g) ( minimum)	Typical Range	Maximum	Design Case
Methane (vol%)	80-100		95.3
Ethane (vol%)	0-10		2.6
Propanes+ (vol%)	0-1	1.5	0.7
Inerts (Co2, N2) (vol%)	0-10		0.7
Oxygen (vol%)		0.2	
Total Sulfur (ppmv)	0-12	20	5

## Operation Support

Utilities for the Production of 100Nm3/h of H2 the following utilities are require :

Natural gas : **41 Nm3/h**  
Municipal water : **105-140 kg/h**  
Cooling Water : **12.5m3**  
Electricity power : **40kW (400V, 3 phases, 50Hz) for combustion air blower, syngas compressor, air coolers, extractor fan (ventilation system) to purge container , feedwater pump, RO water pump and PSA**

## Output Specifications :

Product Flow : **Standard flow 35-200 Nm3/h net hydrogen (up to 500-1,000 Nm3/h upon request)**  
H2 purify : **Typically 99.95% less than 10ppm CO**  
Delivery Pressure : **Typically 11bar(g), up to 40-50bar(g) upon request.**  
Turndown : **40% of design capacity**  
Thermal Efficiency : **approximately 69% (LHV net H2/LHV feed + fuel) or about 398 LHV Btu feed + fuel/net scf H2**

## Dimension

- The system components will be integrated using a high-cube ISO container
- For the production of 50Mn3/h of H2 the container dimensions are 2.44m (wide) x 9m (long) x 2.74m (high)